

## A method for simulating temperature programmed desorption peaks

R. Spinicci\*

Dipartimento di Energetica, Università di Firenze, Via S. Maria 3, 50139 Firenze, Italy

Received 10 May 1996

### Abstract

A procedure for simulating temperature programmed desorption (TPD) peaks is discussed with the aim of determining the shape of a TPD peak and the temperature range, where it is placed, when starting from the knowledge of the peak area (corresponding to the volume of gas adsorbed), of the values of the kinetic parameters (related to the energetic interactions adsorbate–adsorbent), and of some important experimental parameters.

Finally the goodness of the method is checked by simulating a peak at different heating rate and comparing the value of the activation energy, taken as a starting point, with the one that is calculated from the variation of the peak maximum in the temperature scale with the heating rate. © 1997 Elsevier Science B.V.

**Keywords:** Temperature programmed desorption; Peak simulation; Kinetic analysis

### 1. Introduction

When performing kinetic evaluation in temperature programmed desorption experiments, the starting point is always the exploitation of the general equation:

$$-\frac{d\theta}{dt} = k \cdot f(\theta)$$

which relates the rate of desorption  $-(d\theta/dt)$  to some function of the fractional surface coverage,  $\theta$ , through the rate constant  $k$ , which is governed by the Arrhenius equation:

$$k = A \cdot e^{-E/RT}$$

where,  $E$  is the activation energy associated with the process and  $A$  is the pre-exponential factor. The

function  $f(\theta)$  is usually not known and can provide useful information about the mechanism of the desorption and therefore about the mechanism of adsorption itself.

As reported elsewhere [1], there is the possibility of deducing the function  $f(\theta)$  and the kinetic parameters by analysing a single peak: the above equation of the rate of desorption can be rewritten in the form:

$$h_t = k \cdot f\left(\frac{A - A_t}{A}\right),$$

by taking into account that at every instant of the desorption process, the peak height  $h_t$  is proportional to the rate of desorption and the fractional surface coverage  $\theta$  to be uncovered is proportional to the ratio between the residual area  $(A - A_t)$  and the total peak area  $A$  (Fig. 1).

It is therefore possible to determine, from a single peak, the kinetic mechanism which governs the pro-

\*Corresponding author. Tel.: 972 7 461 474; Fax: 972 7 472944 or 461474; e-mail: jbaram@bgumail.bgu.ac.il.

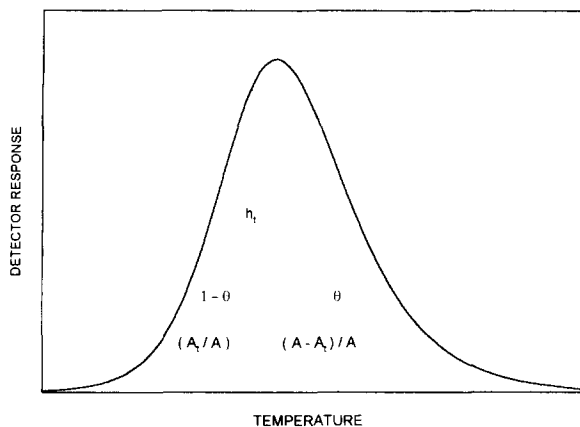


Fig. 1. A simplified TPD peak showing the main peak parameters.

cess, by checking which function can give the best Arrhenius plot. But in some cases, this procedure can give unsatisfactory results, because the straight line does not cover the full range of the fractional surface coverage and it is not possible to distinguish if this discrepancy is due to some experimental problem (for example a not perfect linear heating) or to the occurrence of multiple peaks (for example a central peak with a shoulder).

Therefore, it is useful to reconstruct a TPD peak by a computer calculation starting from the knowledge of the kinetic parameters and of the function  $f(\theta)$ : a theoretical curve of this type can therefore be compared with the experimental peak, improving its kinetic analysis.

The kinetic mechanisms for desorption, which can be investigated, can involve surface heterogeneities and diffusional limitations, but in this analysis only first and second order kinetics, with or without readsorption, will be analysed in order to outline a general method, taking into account that diffusional limitations can be avoided during the experimentation, and that surface heterogeneity is important above all at the beginning of desorption, for large surface coverages.

## 2. Method

As reported in [1], the kinetic equation for a first order desorption (without readsorption):

$$-\frac{d\theta}{dt} = k \cdot \theta$$

can be rearranged and written in the form:

$$h_t = \frac{ZA}{\beta C_s} e^{-E/RT} \left( \frac{A - A_t}{A} \right)$$

where  $h_t$  is the peak height at the time  $t$ , and temperature  $T$ ,  $Z$  is the pre-exponential factor,  $E$  is the activation energy,  $A$  is the total peak area,  $\beta$  is the linear heating rate,  $C_s$  is the chart speed of the strip chart recorder,  $A_t$  is the area developed by the detector signal at the time  $t$  and temperature  $T$ .

The simulation procedure involves the necessity of calculating  $h_t$  only as a function of  $T$ , taking  $Z$  and  $E$  as the starting point. This means to divide the partial area  $A_t$  in two parts, that is the area  $A_{t-1}$  and the trapezoid area  $(h_t + h_{t-1}) \cdot \delta / 2$ , where  $\delta$  is the interval between two points. By approximating the initial heights and therefore the initial areas, it is possible to calculate every height, because  $A_{t-1}$  and  $h_{t-1}$  are always known (Fig. 2). Therefore, since  $A_t = A_{t-1} + [(h_t + h_{t-1}) \cdot \delta] / 2$ , we can write, for first order kinetics, after simple algebraic manipulations:

$$h_t = \frac{(Z/2\beta C_s) \cdot e^{-E/RT} \cdot (2A - 2A_{t-1} - \delta \cdot h_{t-1})}{(1 + (Z\delta/2\beta C_s) \cdot e^{-E/RT})}$$

The kinetic equation for a second order desorption (without readsorption):

$$-\frac{d\theta}{dt} = k \cdot \theta^2$$

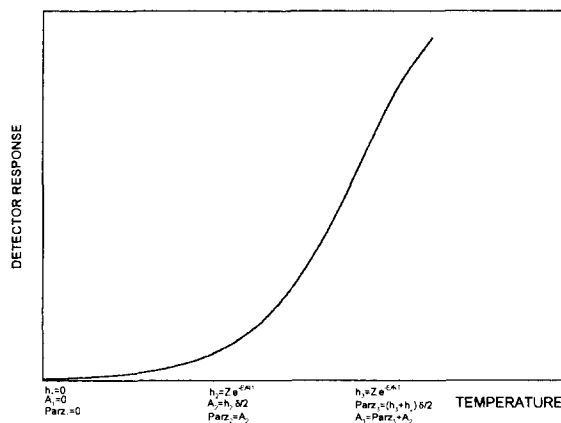


Fig. 2. Analysis of the approximate evaluation of heights and areas at the beginning of the peak.

can be rewritten as:

$$h_t = \frac{ZA}{\beta C_s} e^{-E/RT} \left( \frac{A - A_t}{A} \right)^2$$

and with a similar procedure it is possible to obtain an equation, which relates  $h_t$  and  $T$ :

$$\begin{aligned} & \left( \frac{Z \cdot \delta^2}{4 \cdot A \cdot \beta \cdot C_s} e^{-E/RT} \right) h_t^2 \\ & - \left( 1 + 2\delta \frac{(2A - 2A_{t-1} - \delta h_{t-1}) \cdot Z \cdot e^{-E/RT}}{4 \cdot A \cdot \beta \cdot C_s} \right) h_t \\ & + \left( \frac{(2A - 2A_{t-1} - \delta h_{t-1})^2 \cdot Z \cdot e^{-E/RT}}{4 \cdot A \cdot \beta \cdot C_s} \right) = 0 \end{aligned}$$

This is an equation of second rank and therefore has two solutions, but only one has physical meaning, and it is therefore possible to find the value of  $h_t$  at every predetermined temperature.

The kinetic equation for a first order desorption with readsorption:

$$-\frac{d\theta}{dt} = k \cdot \frac{\theta}{1 - \theta}$$

can be rewritten as:

$$h_t = Z' \cdot e^{\Delta H^0/RT} \left( \frac{A - A_t}{A_t} \right)$$

where  $Z' = [(FC_w A)/(S\beta C_s)]e^{\Delta S^0/R}$  is the “pre-exponential factor” (It must be taken into account that  $F$  is the carrier gas flow rate,  $C_w$  is the recorder chart width, and the  $S$  is the recorder sensitivity.) The elaboration of this equation according to the same criteria allows to obtain a second rank equation in  $h_t$ :

$$\begin{aligned} & \delta \cdot h_t^2 + (\delta Z' e^{-\Delta H^0/RT} + (2A_{t-1} + \delta h_{t-1})) \cdot h_t \\ & - Z' e^{-\Delta H^0/RT} (2A - (2A_{t-1} + \delta h_{t-1})) = 0 \end{aligned}$$

which can be solved by giving, at every temperature, a solution with a physical meaning.

Finally, the fourth case remains to be considered, that is the second order desorption with readsorption. In this case the kinetic equation:

$$-\frac{d\theta}{dt} = k \cdot \left( \frac{\theta}{1 - \theta} \right)^2$$

can be rewritten in the form:

$$h_t = Z' \cdot e^{\Delta H^0/RT} \left( \frac{A - A_t}{A_t} \right)^2$$

The elaboration of this equation leads to an equation of third rank, whose solution is somewhat complex, because the values of  $h_t$  at the beginning of the peak are very small and quite different from those at the centre: the computer procedure must therefore use different numerical methods, according to the range of the value of  $h_t$ .

The equation to be solved (which obviously shows only one solution with physical meaning) is:

$$\begin{aligned} & \delta^2 \cdot h_t^3 + (2\delta I_{t-1} - Z' e^{-\Delta H^0/RT} \delta^2) \cdot h_t^2 \\ & + (I_{t-1}^2 - 2I_{t-1} Z' e^{-\Delta H^0/RT} \delta \\ & + 4AZ' e^{-\Delta H^0/RT} \delta) \cdot h_t \\ & - Z' e^{-\Delta H^0/RT} (I_{t-1}^2 + W_{t-1}) = 0 \end{aligned}$$

where:  $I_{t-1} = 2A_{t-1} + \delta h_{t-1}$  and  $W_{t-1} = 4A^2 - 8AA_{t-1} - 4A\delta h_{t-1}$ .

The computer program therefore, accepts as input data, the total peak area, the recorder chart speed, the interval between two examined points, the heating rate of the catalyst, the starting temperature of the peak and finally the pre-exponential factor (which contains some experimental parameters also) and the activation energy. It allows to choose among the different kinetic mechanism and give as output data heights, lengths (along  $x$ -axis), temperature and areas at every temperature, either on video or in a text file, in order to perform any type of analysis.

Herewith four simulated TPD peaks are shown, each referring to one of these four cases.

1. First order desorption without readsorption (Fig. 3).
2. Second order desorption without readsorption (Fig. 4).
3. First order desorption with readsorption (Fig. 5).
4. Second order desorption with readsorption (Fig. 6).

It is possible to verify the validity of the simulations by means of two procedures. The first lies in determining for each peak the four Arrhenius plots and checking the linearity of the plot corresponding to the proposed kinetic model. As an example it is reported in Fig. 7 the Arrhenius plots for the first order peak of Fig. 3.

It is therefore possible to check that the first order Arrhenius plot shows a good linearity nearly in the

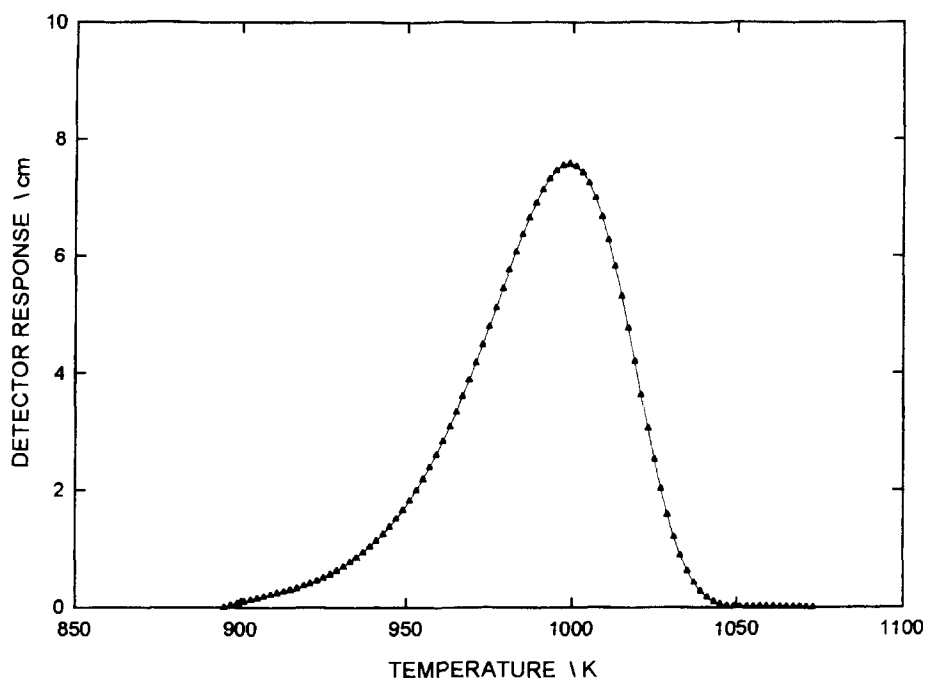


Fig. 3. Simulation of a first order desorption peak.  $A_{\text{tot}}=27 \text{ cm}^2$ ;  $C_s=0.5 \text{ cm min}^{-1}$ ;  $\delta=0.25 \text{ cm}$ ;  $\beta=8^\circ\text{C min}^{-1}$ ;  $T_i=895 \text{ K}$ ;  $E_{\text{att}}=377770 \text{ J mol}^{-1}$ ;  $Z=1.66 \times 10^{20}$ .

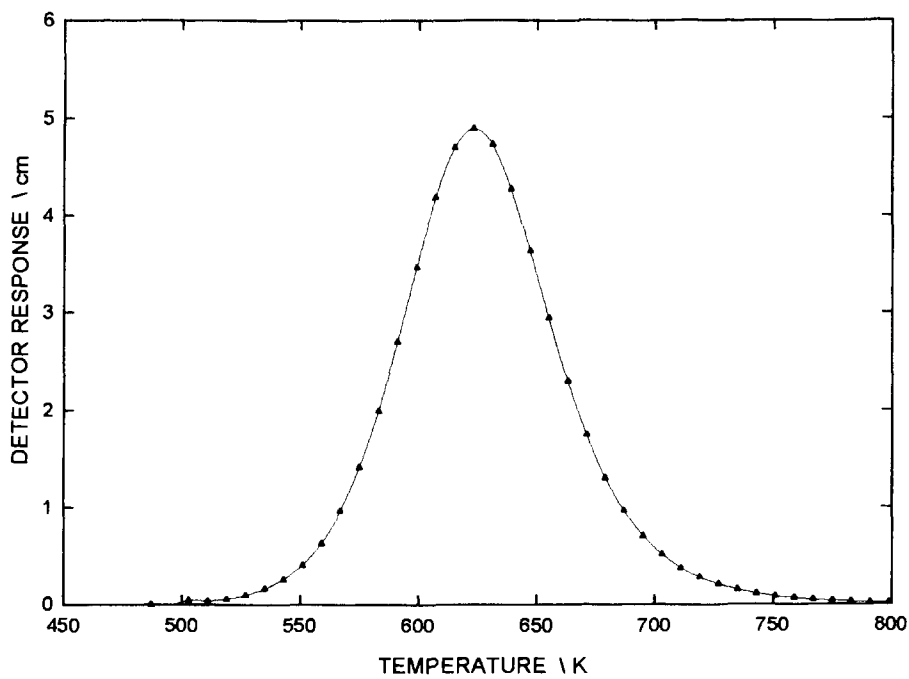


Fig. 4. Simulation of a second order desorption peak.  $A_{\text{tot}}=25.3 \text{ cm}^2$ ;  $C_s=0.5 \text{ cm min}^{-1}$ ;  $\delta=0.5 \text{ cm}$ ;  $\beta=8^\circ\text{C min}^{-1}$ ;  $T_i=487 \text{ K}$ ;  $E_{\text{att}}=146300 \text{ J mol}^{-1}$ ;  $Z=2.5 \times 10^{12}$ .

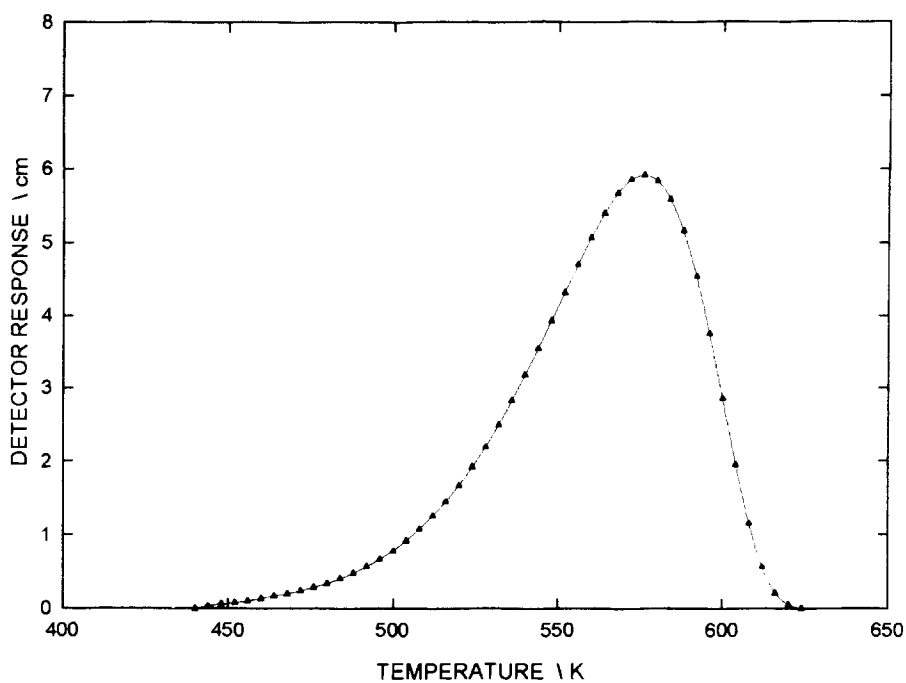


Fig. 5. Simulation of a first order desorption peak with readsorption.  $A_{\text{tot}}=25 \text{ cm}^2$ ;  $C_s=0.5 \text{ cm min}^{-1}$ ;  $\delta=0.25 \text{ cm}$ ;  $\beta=8^\circ\text{C min}^{-1}$ ;  $T_i=440 \text{ K}$ ;  $H^0=180\,000 \text{ J mol}^{-1}$ ;  $\ln Z=40$ .

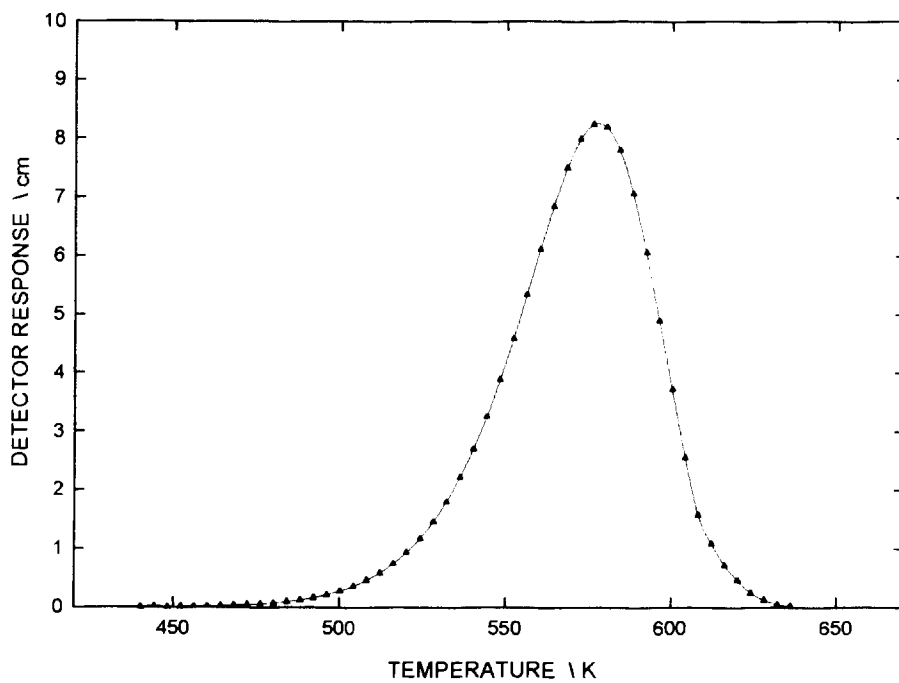


Fig. 6. Simulation of a second order desorption peak with readsorption.  $A_{\text{tot}}=28.2 \text{ cm}^2$ ;  $C_s=0.5 \text{ cm min}^{-1}$ ;  $\delta=0.25 \text{ cm}$ ;  $\beta=8^\circ\text{C min}^{-1}$ ;  $T_i=440.2 \text{ K}$ ;  $\Delta H^0=125\,000 \text{ J mol}^{-1}$ ;  $\ln Z=89.9$ .

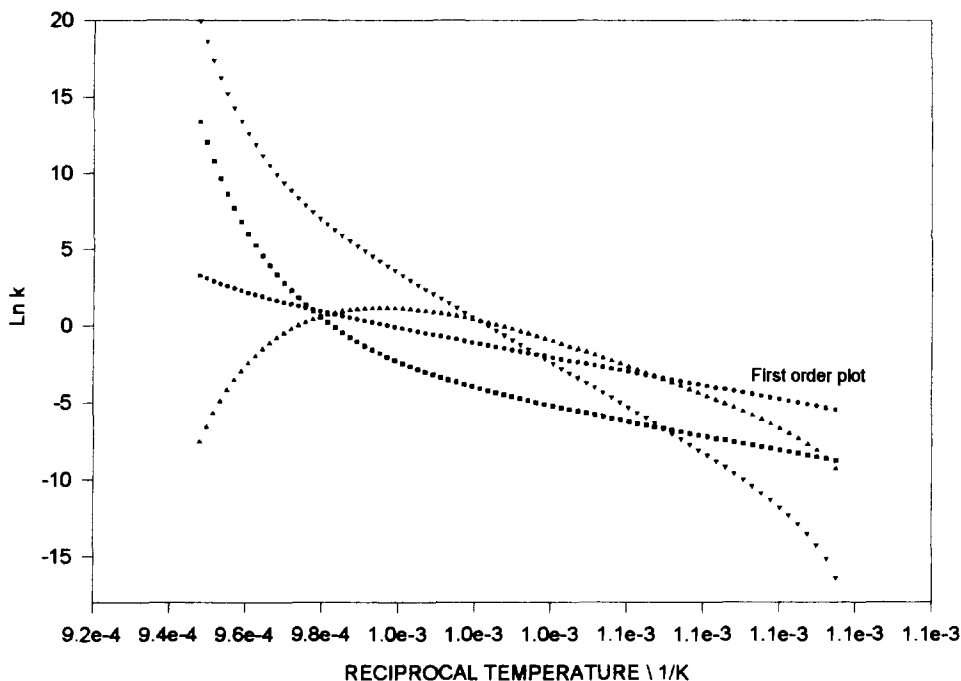


Fig. 7. Arrhenius plots for the first order desorption illustrated in Fig. 3. The slope gives the value of  $-E/R$  and the intercept on the ordinate gives the logarithm of pre-exponential factor.

complete range of the temperatures, that is of the surface coverage.

By means of closer examinations it is possible to see that the linearity of the first order plot ranges from  $\theta=1$  to  $\theta=0.015$ , and therefore it is possible to conclude that the desorption fits the model of the first order kinetics in the *entire* range of fractional surface coverage.

The other Arrhenius plots are evidently not linear in all range of the fractional surface coverage or in a large part of that.

The calculations of the activation energy and of the pre-exponential factor give values in complete agreement with the starting values of the simulation, that is  $E_{\text{att}}=375\,000 \text{ J mol}^{-1}$  and  $Z=1.5 \times 10^{19}$ .

The second procedure is based on simulating the same peak at three different heating rates, as shown in Figs. 8 and 9 for the simulated first order peak of Fig. 3.

Keeping in mind that it is possible to exploit the method based on the heating rate variation [2] and therefore by plotting the value of  $(2 \ln T_M - \ln \beta)$  versus  $1/T_M$ , an activation energy of  $380\,200 \text{ J mol}^{-1}$

and a pre-exponential factor of  $2.8 \times 10^{19}$  have been found, in good agreement with the starting values used for the simulation.

### 3. Conclusions

The kinetic analysis of a temperature programmed desorption peak is a procedure which can give in many cases, unreliable results. The widely used analysis of the peak maximum temperature shift with increasing heating rate is sensitive to minor experimental errors, such as slight differences in surface coverage [3]. But, above all, different heating rates can affect up to different extent some physical and chemical factors, such as for example thermal lag and eventual readorption.

Keeping in mind that it is very important optimising the instrumental apparatus, the analysis of a single peak appears therefore more reliable; in this perspective the reconstruction of a theoretical peak can be important from a practical point of view because it allows to distinguish the different effect of the kinetic

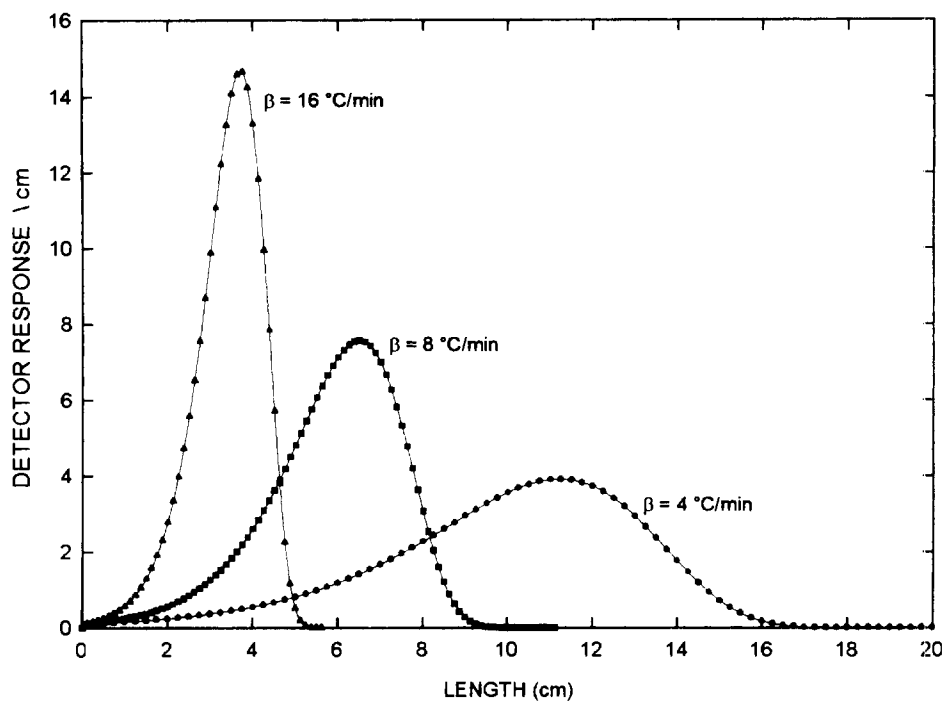


Fig. 8. Simulation at three different heating rates of a first order peak: the peaks are reported as function of the axis length (expressed in cm.), in order to see the invariance of the total area.

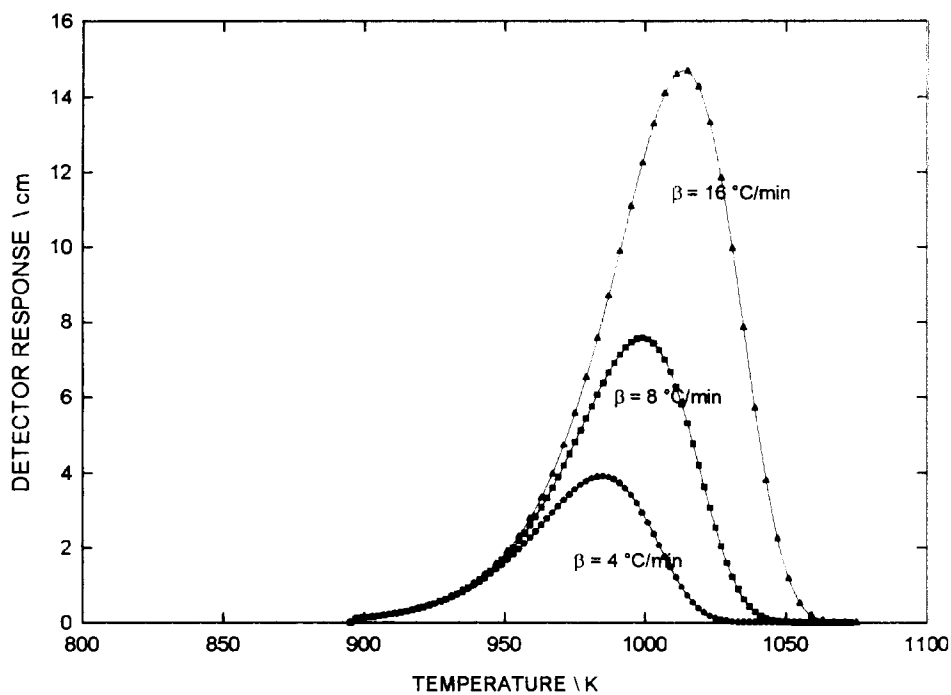


Fig. 9. Simulation at three different heating rates of a first order peak: the peaks are reported as function of the temperature. in order to see the shift towards higher temperature of  $T_M$ .

order of the pre-exponential factor and of the activation energy on the shape of the peak.

It is possible to compare an experimental peak with a theoretical one and to infer the existence of diffusional effects or to define the presence of multiple peaks, due to desorption of different adsorbed species.

## Appendix

### LIST OF THE PROGRAM TPD.BAS

10	COLOR 7,1	320	DIM HZ(280)
20	CLS	330	DIM HU(280)
30	PRINT. PRINT. PRINT'PRINT: PRINT:	340	DIM HV(280)
	PRINT	350	OPEN "O",#1, "TPD.DAT"
40	PRINT "SIMULATION OF A TPD PEAK	360	REM
	DESCRIBED BY 1st OR 2nd ORDER	370	REM DATA INPUT
	KINETICS"	380	REM
50	PRINT:PRINT	390	CLS
60	PRINT "by"	400	INPUT "The peak total area is (cmq) : ":A
70	PRINT:PRINT	410	PRINT
80	PRINT "Roberto Spinicci"	420	INPUT "The recorder chart speed is (cm/
90	PRINT: PRINT: PRINT: PRINT: PRINT:		min) :": CS
	PRINT: PRINT: INPUT "Press a key to	430	PRINT:
	continue"; Q\$	440	INPUT "The interval between two exam-
100	IF Q\$="s" THEN GOTO 140		ined point is (cm) :";DELTA
110	DEFDBL A–H	450	PRINT
120	DEFINT I	460	INPUT "The heating rate of the catalyst
130	DEFDBL J–Z		sample is (K/min) :"; BETA
140	DIM ALT(280)	470	PRINT
150	DIM AREA(280)	480	INPUT "The starting temperature of the
160	DIM TEMP(280)		peak is (K) : "; TT
170	DIM X(280)	490	PRINT
180	DIM Y(280)	500	PRINT " You must input now the
190	DIM PARZ(280)		preexponential factor. Remember that for
200	DIM W(280)		desorption with readsorption this term
210	DIM ALFA(280)	510	expresses: $\ln(F * C_w / S) * \exp(DS \phi / R)$ "
220	DIM OTA(280)		PRINT
230	DIM ETA(280)	520	INPUT "The preexponential factor is :"; Z
240	DIM J(280)	530	PRINT
250	DIM HA(280)	540	INPUT "The activation energy or (in case
260	DIM HB(280)		of desorption with readsorption, the heat
270	DIM HC(280)		of adsorption is (J/mol) : ";ATT
280	DIM HQ(280)	550	PRINT
290	DIM HD(280)	560	REM
300	DIM HR(280)	570	REM CHOICE OF THE DESORPTION
310	DIM HT(280)		KINETIC ORDER
		580	REM
		590	INPUT "The kinetic order is :"; N
		600	PRINT
		610	CLS
		620	PRINT: PRINT: PRINT: PRINT: PRINT:
			PRINT: PRINT: "You can choose the type
			of kinetic mechanism"; PRINT "with or
			without readsorption"; PRINT "and start
			the simulation.";
		630	PRINT: PRINT: PRINT: PRINT: PRINT:
			PRINT
		640	IF N=2 GOTO 1420



```

650 REM
660 REM CHOICE BETWEEN A KINETICS
    OF 1ST ORDER WITHOUT OR WITH
    READSORPTION
670 REM
680 INPUT "The kinetics is affected by read-
    sorption?"; CS
690 IF CS="y" GOTO 950
700 CLS
710 PRINT: PRINT: PRINT: PRINT: PRINT:
    'PRINT
720 PRINT "Now the program is performing
    the calculations of heights, partial areas
    and of temperatures of the peak, for a
    kinetics of 1st ORDER WITHOUT
    READSORPTION, then it is writing the
    related values in the file TPD.DAT and
    show them on video"
730 PRINT: PRINT: PRINT: PRINT: PRINT:
    PRINT: PRINT: PRINT: PRINT: PRINT:
    PRINT: PRINT: PRINT: INPUT " Press a
    key to continue"; Q$
740 IF Q$="y" THEN GOTO 750
750 REM
760 REM CALCULATION OF A PEAK OF
    1ST ORDER WITHOUT READSORP-
    TION
770 REM
780 TEMP(1)=TT
790 ALT(1)=0
800 AREA(1)=0
810 X(1)=0
820 PARZ(1)=AREA(1)
830 FOR I=2 TO 280
840 CONTATOR=1
850 TEMP(I)=TEMP(I-1)+ (DELTA*BE-
    TA/CS)
860 Y(I)=(Z/2*BETA*CS))*(EXP(-ATT/
    (8.314*TEMP(I))))
870 W(I)=(2*A)-(2*AREA(I-1))-(ALT
    (I-1)*DELTA)
880 ALT(I)=W(I)*Y(I)/(1+(Y(I)*DELTA))
890 PARZ(I)=(ALT(I)+ALT(I-1))*
    DELTA/2
900 AREA(I)=AREA(I-1)+PARZ(I)
910 X(I)=X(I-1)+DELTA
920 IF AREA(I)=>A THEN GOTO 940
930 NEXT I
940 GOTO 1210
950 CLS
960 PRINT: PRINT: PRINT: PRINT: PRINT:
    PRINT
970 PRINT "Now the program is performing
    the calculations of heights, partial areas
    and of temperatures of the peak, for a
    kinetics of 1st ORDER WITH READ-
    SORPTION; then it is writing the related
    values in the file TPD.DAT and show them
    on video"
980 PRINT: PRINT: PRINT: PRINT: PRINT:
    PRINT: PRINT: PRINT: PRINT: PRINT:
    PRINT: PRINT: PRINT: INPUT" Press a
    key to continue"; Q$
990 IF Q$="y" THEN GOTO 1000
1000 REM
1010 REM CALCULATION OF A PEAK OF
    1ST ORDER WITH READSORPTION
1020 REM
1030 TEMP(1)=TT
1040 ALT(1)=0
1050 X(1)=0
1060 AREA(1)=0
1070 PARZ(1)=AREA(1)
1080 FOR I=2 TO 280
1090 CONTATOR=I
1100 TEMP(I)=TEMP(I-1)+ (DELTA*BE-
    TA/CS)
1110 ALF(I)=EXP(Z-(ATT/(8.314*TEM-
    P(I))))
1120 Y(I)=DELTA*ALT(I-1)+2*AREA(I-1)
1130 W(I)=Y(I)+ALF(I)*DELTA
1140 J(I)=ALF(I)*(2*A-Y(I))
1150 ALT(I)=(-W(I)+SQR((W(I)^2)+
    4*DELTA*J(I)))/(2*DELTA)
1160 PARZ(I)=(ALT(I)+ALT(I-1))*DELTA/2
1170 AREA(I)=AREA(I-1)+PARZ(I)
1170 X(I)=X(I-1)+DELTA
1190 IF AREA(I)=>A THEN GOTO 1210
1200 NEXT I
1210 CLS
1220 REM
1230 REM PRINTING ON VIDEO AND
    WRITING IN THE FILE OF THE CAL-
    CULATED PARAMETERS
1240 REM
1250 PRINT

```

```

1260 PRINT TAB(5);"HEIGHTS"; TAB(22);
      "LENGTHS"; TAB(36); "AREAS";
      TAB(54); "TEMPERATURES"
1270 PRINT
1280 FOR I=1 TO CONTATOR
1290 PRINT TAB (1); ALT(I); TAB(25); X(I);
      TAB(32); AREA(I); TAB(55); TEMP(I)
1300 WRITE#1, X(I); ALT(I); AREA(I); TEM-
      P(I)
1310 NEXT I
1320 WRITE # 1, CONTATOR
1330 CLOSE # 1
1340 INPUT "Do you want to see the TPD
      peak?"; B$
1350 IF B$="N" GOTO 2480
1360 GOSUB 2760
1370 INPUT "Do you want to print the obtained
      results? (y/n)"; Z$
1380 IF Z$="N"GOTO 1400
1390 GOSUB 2520
1400 END
1410 PRINT
1420 INPUT "The kinetics is affected by read-
      sorption? (y/n)"; C$
1430 REM
1440 REM CHOICE BETWEEN THE KI-
      NETICS OF 2ND ORDER WITH OR
      WITHOUT READSORPTION
1450 REM
1460 CLS
1470 IF C$="Y" GOTO 1750
1480 PRINT: PRINT: PRINT: PRINT: PRINT:
      PRINT
1490 PRINT "Now the program is performing the
      calculations of heights, partial a readsorp-
      tion and of temperatures of the peak, for a
      kinetics of 2nd order without readsorption
      then it is writing the related values in the
      file TPD.DAT and show them on video"
1500 PRINT: PRINT: PRINT: PRINT: PRINT:
      PRINT: PRINT: PRINT: PRINT : PRINT:
      PRINT: PRINT: PRINT: INPUT" Press a
      key to continue"; Q$
1510 IF Q$="y" THEN GOTO 1520
1520 REM
1530 REM CALCULATION OF A PEAK OF
      SECOND ORDER WITHOUT READ-
      SORPTION
1540 REM
1550 COST=Z/(4*BETA*CS*A)
1560 TEMP(1)=TT
1570 ALT(1)=0
1580 AREA(1)=0
1590 X(1)=0
1600 PARZ(1)=AREA(1)
1610 FOR I=2 TO 280
1620 CONTATOR=I
1630 TEMP(I)=TEMP(I-1)+(DELTA*BETA/
      CS)
1640 ALF(I)=EXP(-ATT/(8.314*TEMP(I)))
1650 W(I)=(2*A)-(2*AREA(I-1))-(ALT
      (I-1)*DELTA)
1660 Y(I)=2*DELTA*W(I)*COST*ALFA
      (I)+1
1670 J(I)=COST*ALFA(I)* W((I)^2)
1680 ALT(I)=(Y(I)-(SQR(Y(I)^2-4*J(I)*
      (DELTA^2)*COST*ALFA(I))))/(2*COS-
      T*ALFA(I)*DELTA^2))
1690 PARZ(I)=(ALT(I)+ALT(I-1))*DELTA/2
1700 AREA(I)=AREA(I-1)+PARZ (I)
1710 X(I)=X(I-1)+DELTA
1720 IF A-AREA(I)<.01 THEN GOTO 1740
1730 NEXT I
1740 GOTO 2320
1750 PRINT: PRINT: PRINT: PRINT: PRINT:
      PRINT:
1760 PRINT "Now the program is performing
      the calculations of heights, partial areas
      and of temperature of the peak, for a
      kinetics of 2nd ORDER WITH READ-
      SORPTION; then it is writing the related
      values in the file TPD.DAT and show them
      on video"
1770 PRINT: PRINT: PRINT: PRINT: PRINT:
      PRINT: PRINT: PRINT: PRINT : PRINT:
      PRINT: PRINT: PRINT: INPUT" Press a
      key to continue"; Q$
1780 IF Q$="s" THEN GOTO 1790
1790 REM
1800 REM CALCULATION OF A PEAK OF
      SECOND ORDER WITH READSORP-
      TION
1810 REM
1820 TEMP (1)=TT
1830 ALT(1)=0
1840 AREA(1)=0

```

```

1850 X(1)=0
1860 PARZ(1)=AREA(1)
1870 FOR I=2 TO 280
1880 CONTATOR=I
1890 TEMP(I)=TEMP(I-1)+(DELTA*BETA/
CS)
1900 ALFA(I)=EXP(Z-(ATT/(8.314*TEM-
P))))
1910 Y(I-1)=2*AREA(I-1)+DELTA*ALT
(I-1)
1920 W(I-1)=4*(A^2-2*A*AREA(I-1)-A*
DELTA*ALT(I-1))
1930 REM Solving the 3rd rank equation: x^3+
HA*x^2+HB*x+HC=0
1940 HA(I)=(1/DELTA)*(2*Y(I-1)-DELTA*
ALFA(I))
1950 HB(I)=(1/(DELTA^2))*((Y(I-1)^2)- 2*
DELTA*ALFA(I)*Y(I-1)+4*ALFA
(I)*A*DELTA)
1960 HC(I)=- (ALFA(I)/(DELTA^2))*((Y
(I-1)^2)+W(I-1))
1970 HQ(I)=(3*HB(I)-HA(I)^2)/9
1980 HR(I)=(9*HA(I)*HB(I)-27*HC(I)-2*
(HA(I)^3))/54
1990 REM Calculation of the equation discri-
minant,HD
2000 HD(I)=HQ(I)^3+HR(I)^2
2010 IF HD(I)<0 THEN GOTO 2090
2020 REM Calculation of the real root, when
HD is equal to zero or positive
2030 HZ(I)=HR(I)-SQR(HD(I)): HU(1)=
HR(I)+SQR(HD(I))
2040 HT(I)=EXP(LOG(ABS(HZ(I)))/3)
2050 IF HZ(I)<0 THEN HT(I)=-HT(I)
2060 HV(I)=EXP(LOG(ABS(HU(I)))/3)
2070 IF HU(I)<0 THEN HV(I)=-HV(I)
2080 ALT(I)=HV(I)+HT(I)-HA(I)/3: GOTO
2250
2090 REM Calculation of the real root, when
HD is negative
2100 COEFF=HR(I)/(SQR(-HQ(I)^3))
2110 IF COEFF>.9 GOTO 2160
2120 ALT 1 =2 * S Q R ( -H Q ( I ) ) * C O S
(3.141592654#/6-COEFF^7*5/336-
COEFF^5/40-COEFF^3/18-COEFF/3)-
HA(I)/3
2130 ALT 2 =2 * S Q R ( -H Q ( I ) ) * C O S
((3.141592654#/6-COEFF^7*5/336-
COEFF^5/40-COEFF^3/18-COEFF/3)-
+120*3.141592654#/180)-HA(I)/3
2140 ALT 3 =2 * S Q R ( -H Q ( I ) ) * C O S
((3.141592654#/6-COEFF^7*5/336-
COEFF^5/40-COEFF^3/18-COEFF/3)-
+240*3.141592654#/180)-HA(I)/3
2150 GOTO 2200
2160 IF COEFF>.9999999 THEN COEFF=
.9999999
2170 ALT1=2*SQR(-HQ(I))*COS ((SQR(1-
COEFF^2))/3)-HA(I)/3
2180 ALT2=2*SQR(-HQ(I))*COS ((SQR(1-
COEFF^2))/3)+120*3.141592654#/180)-
HA(I)/3
2190 ALT3=2*SQR(-HQ(I))*COS ((SQR(1-
COEFF^2))/3)+240*3.141592654#/180)-
HA(I)/3

```

## References

- [1] R. Spinicci, J. Therm. Anal., 29 (1984) 1061.
- [2] J.L. Falconer and J.A. Schwarz, Catal. Rev. -Sci. Eng., 25 (1983) 141.
- [3] A. Brenner and D.A. Hucul, J. Catal., 56 (1979) 134.